

## CLAIMS

1. A crystalline mixture solid composition comprising  
α-D-glucopyranosyl-1,1-mannitol,  
5 α-D-glucopyranosyl-1,6-sorbitol and 0.01 to 1.99 wt% of  
α-D-glucopyranosyl-1,1-sorbitol (the above wt% is based on  
the total weight of the α-D-glucopyranosyl-1,1-mannitol,  
α-D-glucopyranosyl-1,6-sorbitol and  
α-D-glucopyranosyl-1,1-sorbitol).

10 2. A crystalline mixture solid composition comprising 50  
to 98 wt% of α-D-glucopyranosyl-1,1-mannitol, 1 to 50 wt%  
of α-D-glucopyranosyl-1,6-sorbitol and 0.01 to 1.99 wt% of  
α-D-glucopyranosyl-1,1-sorbitol (the above wt% is based on  
15 the total weight of the α-D-glucopyranosyl-1,1-mannitol,  
α-D-glucopyranosyl-1,6-sorbitol and  
α-D-glucopyranosyl-1,1-sorbitol).

3. The crystalline mixture solid composition of claim 1  
20 or 2 which comprises 0.01 to 1.5 wt% of  
α-D-glucopyranosyl-1,1-sorbitol.

4. A crystalline mixture solid composition which is thin  
scale and comprises α-D-glucopyranosyl-1,1-mannitol and  
25 α-D-glucopyranosyl-1,6-sorbitol.

5. The crystalline mixture solid composition of claim 4  
which has a specific surface area of 0.1 to 5.0 m<sup>2</sup>/g.

30 6. A process for producing a crystalline mixture solid  
composition, comprising the steps of supplying a composition  
comprising 50 to 80 wt% of α-D-glucopyranosyl-1,1-mannitol,  
1 to 50 wt% of α-D-glucopyranosyl-1,6-sorbitol and 0.01 to  
20 wt% of α-D-glucopyranosyl-1,1-sorbitol into a kneader to

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knead and cool it so as to produce a composition, mixing the composition with a hydrophilic solvent, and separating solid matter from a liquid (the above wt% is based on the total weight of the  $\alpha$ -D-glucopyranosyl-1,1-mannitol,

5  $\alpha$ -D-glucopyranosyl-1,6-sorbitol and  
 $\alpha$ -D-glucopyranosyl-1,1-sorbitol).

7. A process for producing a crystalline mixture solid composition, comprising the steps of supplying a composition comprising 50 to 80 wt% of  $\alpha$ -D-glucopyranosyl-1,1-mannitol, 1 to 50 wt% of  $\alpha$ -D-glucopyranosyl-1,6-sorbitol and 0.01 to 20 wt% of  $\alpha$ -D-glucopyranosyl-1,1-sorbitol into an kneader having a thin and long cooling/kneading zone to knead and cool it, extruding the kneaded product through a punching plate, cooling and grinding the extruded molded product to produce a powdery crystalline mixture solid composition, mixing the composition with a hydrophilic solvent, and separating solid matter from a liquid (the above wt% is based on the total weight of the  $\alpha$ -D-glucopyranosyl-1,1-mannitol,

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20  $\alpha$ -D-glucopyranosyl-1,6-sorbitol and  
 $\alpha$ -D-glucopyranosyl-1,1-sorbitol).

8. A process for producing a crystalline mixture solid composition, comprising the steps of mixing a hydrophilic solvent with an aqueous solution which comprises 50 to 80 wt% of  $\alpha$ -D-glucopyranosyl-1,1-mannitol, 1 to 50 wt% of  $\alpha$ -D-glucopyranosyl-1,6-sorbitol and 0 to 20 wt% of  $\alpha$ -D-glucopyranosyl-1,1-sorbitol, and separating the formed precipitate from a liquid (the above wt% is based on the total weight of the  $\alpha$ -D-glucopyranosyl-1,1-mannitol,

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$\alpha$ -D-glucopyranosyl-1,6-sorbitol and  
 $\alpha$ -D-glucopyranosyl-1,1-sorbitol).

9. The process for producing a crystalline mixture solid

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composition of any one of claims 6, 7 and 8, wherein the hydrophilic solvent is ethanol.

10. The process for producing a crystalline mixture solid  
5 composition of any one of claims 6, 7 and 8, wherein the hydrophilic solvent is an ethanol aqueous solution having a concentration of 60 to 90 %.

11. The crystalline mixture solid composition of any one  
10 of claims 1, 2 and 3 produced by the production process of any one of claims 6, 7 and 8.

12. The crystalline mixture solid composition of claim 4 or 5 produced by the production process of claim 8.